1971 OPERATING SUMMARY

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PARRY SOUND

WATER POLLUTION CONTROL PLANT

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Water management in Ontario

Ontario Water Resources Commission

We are pleased to submit for your consideration a summary of operation during 1971 of the water pollution control plant serving your community.

This operating summary contains parameters normally used to measure plant performance and loading, as well as relevant cost data. Because of the concern over eutrophication of our lakes and of the requirement, in many parts of Ontario, to remove the major contributing factor, results of analysis for phosphorus appear in this summary.

D.S. Caverly,

General Manager.

D. A. McTavish, P. Eng.,

Director,

Division of Plant Operations.

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135 St. Clair Avenue West Toronto 195

PARRY SOUND WATER POLLUTION CONTROL PLANT

operated for

THE TOWN OF PARRY SOUND

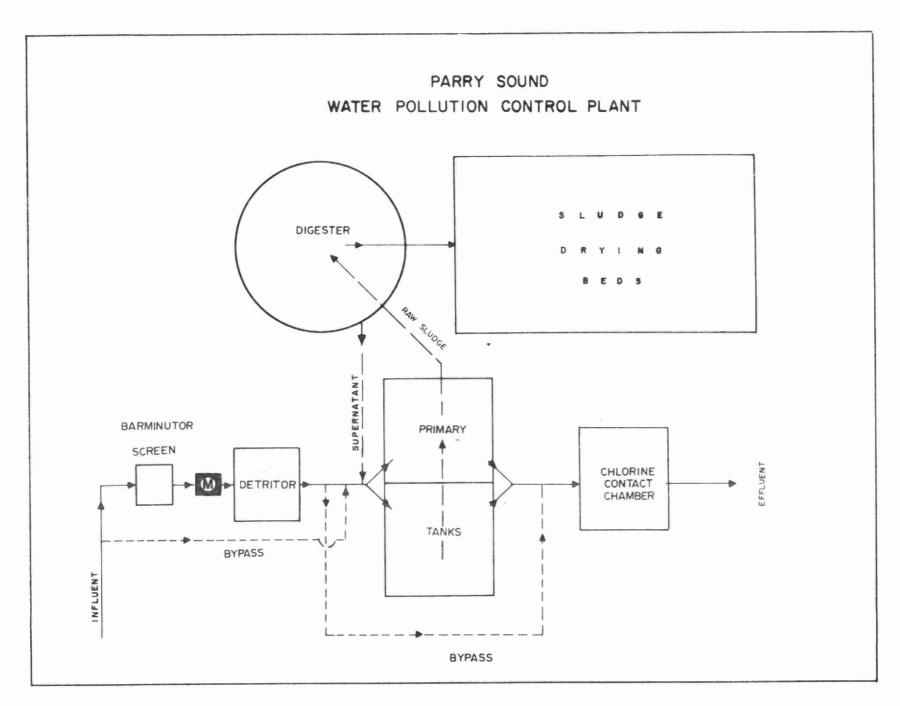
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ONTARIO WATER RESOURCES COMMISSION

1971 ANNUAL OPERATING SUMMARY

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DESIGN DATA

PROJECT NO.	2-0113-62	Primary Sedimentation	PUMPING STATIONS
TREATMENT	Primary	Type: Dorr	#2 Ejector Station
DESIGN FLOW	0.83 mgd	Size: Two 30' x 30' x 10' swd (112,000 gallons) Retention: 3.24 hr	Type: Smith & Loveless Size: One 100 gpm @ 135' tdh
DESIGN POPULATION	7,500	Loading: Surface, 460 gal/ft ² /day Weir, 3700 gal/ft/day	#1 Pumping Station
BOD - Raw Sewage - Removal	250 mg/1 35%	CHLORINATION	Type: Flygt Size: Two 40 gpm @ 26' tdh
SS - Raw Sewage - Removal	200 mg/1 35%	Type: W & T, Type A-731 Size: One 200 lb/day	#7 Pumping Station (Bay St.)
		Chlorine Contact Chamber	Type: Flygt Size: One 40 gpm @ 35' tdh
DDIMADY TOTA TMENT		Size: One $25\frac{1}{2} \times 8\frac{1}{2} \times 8^{1}$ (11, 150 gal)	#3 Pumping Station (Hawthorn Cr.)
PRIMARY TREATMENT Comminution		Retention: 19.2 min OUTFALL	Type: Flygt Size: One 50 gpm
Type: Barminutor Size: One Model C (18")		- to McCurry Lake	#4 Pumping Station (William St.)
Grit Removal		SLUDGE HANDLING	Type: Flygt Size: Two 250 gpm @ 36' tdh
Type: Dorr Detritor		<u>Digestion System</u> - single-stage	#5 Pumping Station (Cascade St.)
Size: One 10 X 10 X 1 ¹ / ₄ Retention: 1.35 min		Type: Dorr draft tubes (2) Size: One 35' dia x 20' 9" swd (20,580 cu ft or 138,000 gal)	Type: Robert Morse (Weinman) Size: Two 420 gpm @ 41' tdh
		Loading: 0.85 lb/cu ft/mo	#6 Pumping Station

Drying Beds

- Four $76\frac{1}{2} \times 29'$

Type: Robert Morse Size: Two 860 gpm @ 150' tdh

71 Review

GENERAL

The project consists of an 0.83 mgd primary treatment plant and nine sewage lift stations, two of which are operated for the Town under an operating agreement. The project is staffed by a chief operator and an operator.

The plant effluent discharged to Georgian Bay, via McCurry Lake and McCurry Creek. During the spring, for a period of two or three weeks after the ice has gone off the lake, strong odours are noted in the proximity of McCurry Lake and McCurry Creek. Intermittent odours are also noted at other times however, are not as strong. A design report to extend and expand the plant to a 1.4 mgd secondary activated sludge plant, and to upgrade pumping stations No. 2 and No. 6 has been received and reviewed. The addition of secondary treatment facilities to the plant will solve the odour problems.

EXPENDITURES

The operating cost for the complete project for the year was \$39, 360.14. The approximate cost per million gallons treated was \$155.00. This compared to \$146.18 in 1970, \$126.66 in 1969 and \$162.39 in 1968.

PLANT FLOWS and CHLORINATION

The average daily flow for the year was 700,000 gallons. The average daily design flow of 830,000 gallons was exceeded 18 percent of the time. A total of 22,000 pounds of chlorine was used during the year, representing an average chlorine dosage of 8.6 mg/l.

PLANT EFFICIENCY

The raw sewage BOD and suspended solids concentrations were respectively 130 mg/l and 185 mg/l. This represented an increase of approximately 5 percent in BOD and 7 percent in suspended solids over the previous year. The final effluent BOD and suspended solids of 64 mg/l and 32 mg/l respectively were similar to last year. The average reduction in BOD was 51 percent and in suspended solids, 32 percent.

A total of 1,073 cubic feet of grit was removed during the year for an average of 4.2 cubic feet per million gallons treated. This compared to figures of 3.8 in 1970 and 4.7 in 1969 and is indicative of combined storm and sanitary sewers.

SLUDGE DIGESTION and DISPOSAL

A total of 249,000 gallons of raw sludge was pumped to the digester and 97,500 gallons of digested sludge removed from the digester to the drying beds. A total of 124 cubic yards of dried sludge was removed from the beds.

The average total solids concentration of the raw sludge was 6.1 percent; the volatile matter concentration, 55 percent. The digested sludge pumped to the drying beds had an average total solids concentration of 7.7 percent of which 45 percent was volatile matter.

CONCLUSIONS

The plant produced a satisfactory effluent for a primary treatment plant. However this was not adequate to prevent odours from developing in McCurry Lake and McCurry Creek.

A design report to extend the treatment facility to provide secondary treatment and to increase the present capacity to 1.3 mgd was received and reviewed. It is anticipated that construction for these works will commence in 1974.

PROJECT COSTS

NET CAPITAL COST (Final)	\$8	839, 907. 73
DEDUCT - Portion financed by CMHC/MDLB (Final)	1	549, 696.21
Long Term Debt to OWRC	\$2	290, 211.52
Debt Retirement Balance at Credit (Sinking Fund) December 31, 1971	\$	<u>42, 694. 79</u>
Net Operating Debt Retirement Reserve Interest Charged		39, 360.14 3, 485.00 3, 915.39 16, 266.09
TOTAL	\$	63, 026, 62
RESERVE ACCOUNT		
Balance @ January 1, 1971	\$	25, 350.24
Deposited by Municipality		3, 915.39
Interest Earned		1, 736.38
	\$	31,002.01
Less Expenditures		
Balance @ December 31, 1971	\$	31,002.01

OPERATING COSTS 1971 COSTS PAYROLL 46 % FUEL POWER 17% • CHEMICALS 10% GENERAL SUPPLIES TOTAL ANNUAL COST EQUIPMENT NET OPERATING ₱ REPAIRS & MAINTENANCE 10 % SUNDRY 2 % DEBT RETIREMENT WATER 5 % RESERVE 6 % ● TRAVEL < 1 % INTEREST 26 % YEARLY OPERATING COSTS SEWAGE TREATED TREATMENT COSTS TOTAL YEAR in million gallons OPERATING COSTS \$ per million gal & per Ib BOD 1967 234.338 \$29,843.67 \$127.35 24 cents 198.76 1968 32, 277. 42 162.39 28 cents 33,021.33 1969 260.7 126.66 29 cents 240.90 1970 37.883.25 157.20 21 cents 1971 254. 39, 360.14 155.00 21 cents

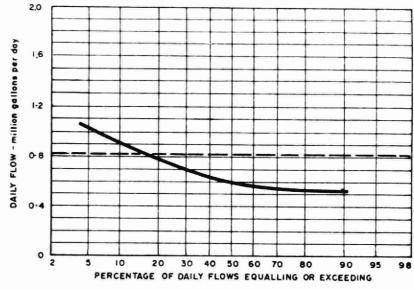
MONTHLY OPERATING COSTS

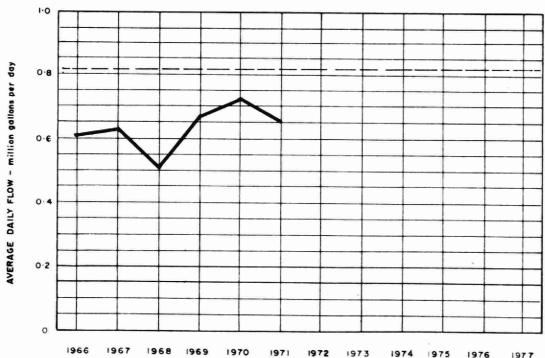
монтн	TOTAL EXPENDITURE	REGULAR PAYROLL	CASUAL PAYROLL	FUEL	POWER	CHEMICALS	GENERAL SUPPLIES	EQUIPMENT	REPAIRS and	SUNDRY*	WATER	TRAVEL
JAN	1519.34	1184.40	-	-	184.89	-	8.00	_	12.37	-	129.68	_
FEB	3736.76	1663.71	-	280.69	533.10	581.18	209.85	-	254.00	62.15	152.08	-
MAR	3419.05	1123.11	-	280.50	507.59	581.18	156.09	-	589.19	43.68	137.71	-
APR	2371.22	1144.99	-	280.50	552.36	_	87.00	_	156.03	16.83	133.51	-
MAY	2938.48	1174.68	132.38	-	693.85	568.50	160.89	-	35.79	25.93	146.46	-
JUNE	3263.26	1281.66	(132.38)	280.50	661.81	568.50	228.02	-	215.20	9.29	150.66	-
JULY	2772.52	1136.96	300.49	-	579.12	-	139.52	-	360.97	114.95	140.51	-
AUG	2413.47	1256.01	308.63	-	540,70	-	112.48	_	-	47.79	147.86	-
SEPT	3776.17	1262.68	108.71	-	532.00	710.65	132.46	183.46	100.17	592.93	153,11	-
ост	2692.62	1885.18	-	-	508.08	-	97.05	-	35.61	21.64	145.06	-
NOV	5051.31	2289.21	-	309.33	543.19	(188.78)	115.22	-	1816.68	30,50	135.96	-
DEC	5405.94	2083.62	-	-	1029.25	1137.00	687.77	-	196.43	11.59	194.04	66.24
TOTAL	39360.14	17486.21	717.83	1431.52	6865.94	3958.23	2134.35	183.46	3772.44	977.28	1766.64	66.24

Brackets indicate credit.

PROCESS DATA	
*	

FLOWS



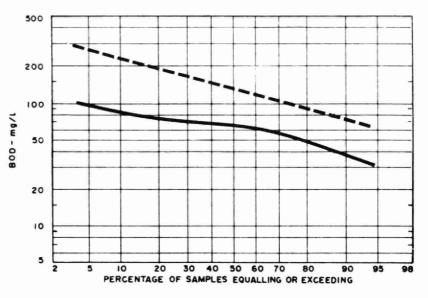


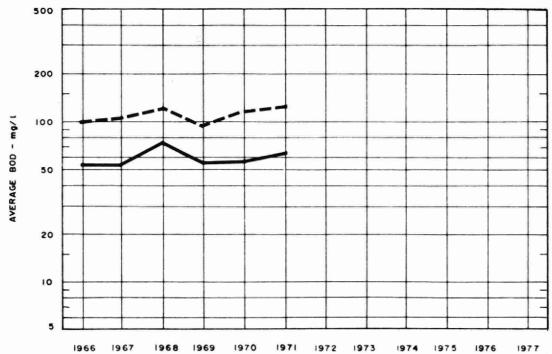
DESIGN CAPACITY _____

PLANT PERFORMANCE

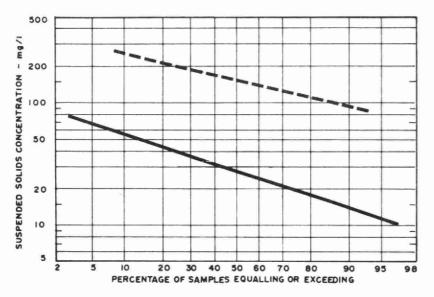
		FLO\	NS		BIOCHEA	AICAL OX	YGEN	DEMAND	SU	SPENDED	SOLID)S	TOTAL	PHOSPHO	ORUS
	TOTAL FLOW	AVERAGE DAY	MAXIMUM		INFLUENT	EFFLUENT	RED	UCTION	INFLUENT	EFFLUENT		UCTION		EFFLUENT	
MONTH	million gallons	mil gal	DAY mil gal	RATE mgd	mg/L	mg/l	%	10 ³ pounds	mg/l	mg/l	%	10 ³ pounds	mg/l as P	mg/l as P	%
JAN	18.	.57	.59	1.0	127	80	36	7.9	175	25	86	26.	-	4.4	-
FEB	17.	.59	.66	1.2	110	75	32	5.8	130	45	65	14.	-	3.8	-
MAR	23.	.75	1.77	2.6	70	49	30	4.9	105	23	78	19.	6.1	3.0	51
APR	40.	1.33	2.20	2.6	100	6	94	37.6	90	5	94	34.	-	1.1	-
MAY	23.	.74	1.26	2.5	147	67	54	18.4	160	28	83	30.	12.0	4.1	66
JUNE	18.	.59	.79	2.6	200	62	69	24.5	460	50	89	73.	9.9	5.0	49
JULY	18.	.57	.86	2.5	200	58	71	25.0	170	25	85	26.	9.2	4.3	53
AUG	18.	.58	.86	2.6	145	63	56	14.6	225	42	81	33.	11.7	5.5	53
SEPT	16.	.54	1.14	2.5	175	80	54	15.3	305	57	81	40.	9.8	5.5	44
ост	17.	.55	.70	2.4	85	45	47	6.9	102	35	66	11.	9.3	4.4	43
NOV	21.	.71	1.03	2.5	120	70	42	10.7	122	30	75	20.	10.4	4.3	59
DEC	25.	. 81	1.30	3.0	100	55	45	11.3	110	20	82	22.	9.0	3.4	62
TOTAL	254.	-	-	-	-	-	-	182.9	-	-	-	348.	-	_	-
AVG.	-	.70	2.20	3.0	130	64	51	15.2	185	33	82	29.	8.5	4.2	51
No. of Samples	-	-	-	-	23	23		-	23	23	-	-	15	23	-

BIOCHEMICAL OXYGEN DEMAND

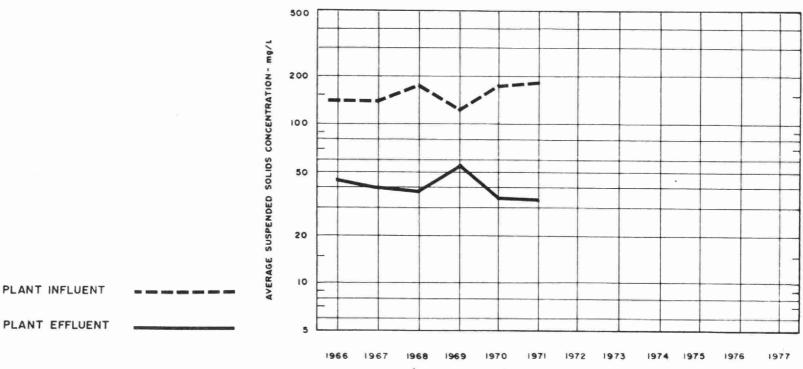




PLANT INFLUENT	
PLANT FEELLIENT	



SUSPENDED SOLIDS

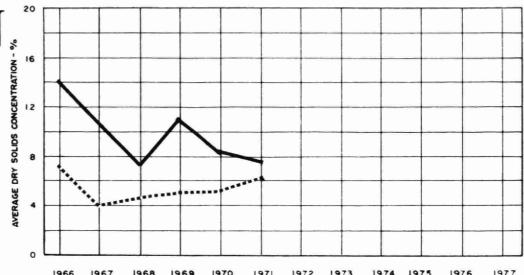


TREATMENT DATA

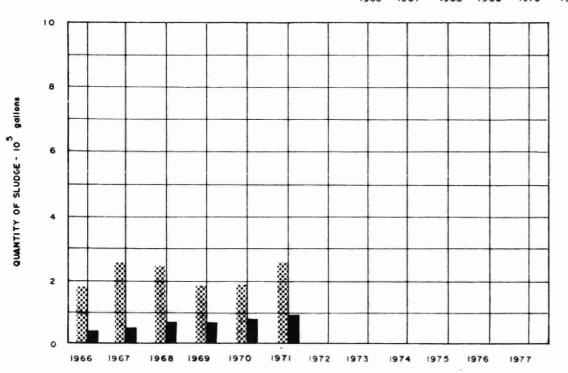
	GRIT	CHLORINA	TION			SLUDGE					
				RAV	V SLUDGE			TED SLUDG		SUPERNATANT	
	QUANTITY REMOVED	CHLORINE USED		QUANTITY	TOTAL	VOLATILE	QUANTITY	TOTAL SOLIDS	VOLATILE SOLIDS	TOTAL SOLIDS	SLUDGE *
монтн		103	DOSAGE	10 3	SOLIDS	SOLIDS	REMOVED IO 3 gallons		1		
	cubic feet	pounds	mg/l	guilons	%	%	gallons	%	%	%	cubic yards
JAN	12	1.8	10.1	17.	5.0	61	9.5	5.9	43	.4	0
FEB	34	1.6	9.4	16.	4.4	66	5.0	6.5	43	.3	0
MAR	66	1.9	7.9	21.	8.6	46	4.5	10.2	70	.3	0
APR	203	1.8	4.6	22.	4.5	43	8.5	9.4	41	.4	22
MAY	52	1.9	8.1	22.	7.1	45	12.0	9.9	39	.6	54
JUNE	104	1.7	9.6	21.	11.6	42	8.0	9.5	34	.3	10
JULY	100	1.7	9.5	22.	8.7	53	8.0	7.4	41	-	13
AUG	91	1.8	10.1	22.	2.9	55	8.0	8.0	42	.2	10
SEPT	76	1.9	11.8	21.	5.2	68	8.0	6.6	36	1.2	8
ост	41	1.9	11.2	22.	5.1	62	8.0	8.4	44	.5	7
NOV	148	2.0	9.2	21.	5.3	63	13.0	7.5	47	1.1	0
DEC	146	2.0	8.1	22.	4.3	57	5.0	3.4	55	1.8	0
TOTAL	1073	22.0	-	249.	(-	-	97.5	-	_	_	124
AVG.	4.2 cubic feet/mil gal	1.8	8.6	21.	6.1	55	8.1	7.7	45	.6	10

^{*} From Drying Beds

DIGESTION %-NOLDS CONCENTRATION SOLDS CONCENTR



DIGESTED SLUDGE .



RAW SLUDGE TO DIGESTER DIGESTED SLUDGE REMOVED

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